# Zeolitic-nanoblock membranes for gas separation

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# Membrane synthesis

• Standard zeolite membranes :

hydrothermal synthesis

with in-situ growth, or seeding and secondary growth

• Our method :

stacking from nano zeolite-precursors from clear solution



# Nano zeolite-precusors

R&D in different groups :

[Tsapatsis], [Schoeman], [Corma], [Martens] :

- In clear solution
- With specific ratio of TPA/SiO<sub>2</sub> in solution
- Existence of precursor nanoparticles of a few nm by SAXS, DLS, TEM, HRTEM, AFM
- Contribute to crystal growth by oriented aggregation
- Structure of precursors in debate :

amorphous or crystalline ?



# Nano zeolite-precursors

• TEM on silicalite clear solution, aged at RT (UAntwerpen)

D. Liang, Van Tendeloo et al, submitted J. Phys. Chem. C.



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# Zeolitic nanoblocks

View of K.U.Leuven

Kirschock et al., Angewandte Chemie, 40, 2637; 2001

- Basic unit = rectangular nanoblock
- Nanoblocks have zeolite-like properties = zeolitic
- Nanoblocks are 4x4x1.3 nm<sup>3</sup>
- Can be used as building units



- 9 short zig/zag channels along a-axis
- 3 long,straigth channels along b-axis
- channels 0.5 nm wide



# Zeogrid powder

Kremer at al., Adv. Funct. Mater., 12, 286, 2002 (KULeuven)

- Nanoblocks can be stacked in an layered way with the use of appropriate surfactants
- Leads to micrometer large grains called zeogrid
- Zeogrid calcined has dual porosity : micropores + interblock voids



# Zeogrid powder

#### N<sub>2</sub> adsorption : **bi-porosity** micropores + supermicropores



#### Low-angle XRD : **no zeolite** layering with repetition of 3<sub>1</sub>nm



| sample        | V(micro)<br>cc/g | V(big micro) cc/g | S(tot) m <sup>2</sup> /g |   |
|---------------|------------------|-------------------|--------------------------|---|
| СТАВ          | 0.14             | 0.53              | 1243                     |   |
| DTAB          | 0.14             | 0.40              | 948                      |   |
| <br>i-SUP2008 |                  |                   |                          | 8 |

# Zeotile powder

Kremer at al., Adv. Mater., 20, 1705, 2003 (KULeuven)





Different way of stacking with the aid of surfactants :  $\downarrow$ Hexagonal stacking of double nanoslab units  $\downarrow$ One dimensional channels of ~3.5 nm

White bar = 10 nm Images: UAntwerpen



## Zeolitic-nanoblock membranes

Zeogrid on porous support :

dipping in solution of nanoblocks + surfactants



Calcination = removal of surfactant/TPA, no crystal growth



#### Zeolitic-nanoblock membranes

Possible advantages :

- thin membranes < 100 nm : high flux, crack free
- bi-porosity : extra high flux
- defect-free + entrance via nanoblock : high selectivity



**Goal : Potential of these membranes ?** 



#### Preliminary tests : Zeolitic-nanoblock film on Si wafer



### Zeolitic-nanoblock membranes

Zeogrid layer on porous support :

- flat and tubular
- α-Al2O3/TiO2 (50-100 nm) + TiO2 (3 nm)

Quality test :

- NF with small PEG's in water (200, 600, 1500 Dalton)
- defect-free membrane has MWCO < 200 D + low flux</li>
- R(1500D) measures defects and supermicropores > 1.5 nm

Current quality on tubes :

• MWCO : 500 à 1000 D, R(1500D) > 95%





# **FESEM** characterisation

on a fracture plane,  $30^{\circ}$  tilt



# **TEM characterisation**





# Adsorption measurements on zeotile/zeogrid powder at RT



# Adsorption measurements on zeogrid powder at RT



powder interesting as CO<sub>2</sub> adsorbent

Measurements: VUB

membranes interesting for CO<sub>2</sub> gas separation

# Single gas separation measurements

| aoc             | Permeability at RT | Permeability at 200°C |
|-----------------|--------------------|-----------------------|
| yas             | (l/hm².bar)        | (l/hm².bar)           |
| N               | M1 : 1290          | M1 : 1800             |
| IN <sub>2</sub> | M2 : 4500          | M2 :                  |
| СЕ.             | M1 : 960           | M1 :                  |
| Sг <sub>6</sub> | M2 : 1950          | M2 :                  |
| Ц               | M1 : 4200          | M1 : 5850             |
| п <sub>2</sub>  | M2 : 11700         | M2 :                  |
| <u> </u>        | M1 : 1500          | M1 : 2100             |
| $UU_2$          | M2:3300            | M2 :                  |

- permeabilities independant of TMP
- 1000 l/hm<sup>2</sup>bar = 1,24 10<sup>-7</sup> mol/m<sup>2</sup>sPa

- ~ Knudsen permselectivities
- permeabilities increase with T



#### Double gas separation measurements

| gas                                   | Selectivity | Permeability at RT<br>(l/hm².bar) |
|---------------------------------------|-------------|-----------------------------------|
| N <sub>2</sub> /CO <sub>2</sub> 88/12 | 0.6 (1.25)  | 3000                              |
| H <sub>2</sub> /CO <sub>2</sub> 40/60 | 1.7 (4.7)   | 9000                              |

Permeate side : P = 1 atm TMP = 1 or 2 bar CO<sub>2</sub> adsorption High fluxes Low selectivities

# Conclusions for zeolitic membranes

- SEM/TEM show nice membranes with clear bi-porosity
- Current quality : 500 à 1000 D, R(1500D) > 95%
- Adsorption on powder shows extra high CO<sub>2</sub> capacity at high pressures : <u>clear potential</u>
- First gas separation results :
  - Single gas separation shows
    - ~ Knudsen behavior, high fluxes increasing with T
  - Double gas separation at low pressure shows
    CO<sub>2</sub> adsorption, high fluxes
- Gas separation measurements at high pressure planned

