Organic Solvent Nanofiltration A New Technology for Molecular Separations

Andrew Livingston, Professor of Chemical Engineering, Imperial College London, UK

- OSN An Emerging Technology
- Membrane Characterisation
- OSN Applications
- Next Generation Membranes

Also:

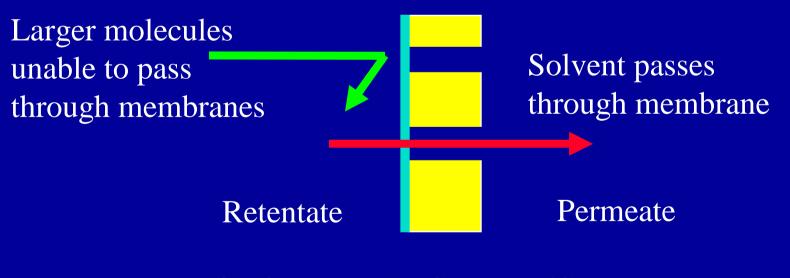
Managing Director Membrane Extraction Technology Ltd www.membrane-extraction-technology.com

Imperial College London





- Nanofiltration membranes are capable of discriminating between molecules in MW range 200-1000 Da
- Applications have been based in aqueous systems
- IF nanofiltration could be applied to separations in organic liquids, could be worth billions of dollars



Rejection R = (1- (Cpermeate/Cretentate)) 100% = perfect rejection; 0% = no separation

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Vision 2020: 2000 Separations Roadmap

Published by the Center for Waste Reduction Technologies of the

In cooperation wit

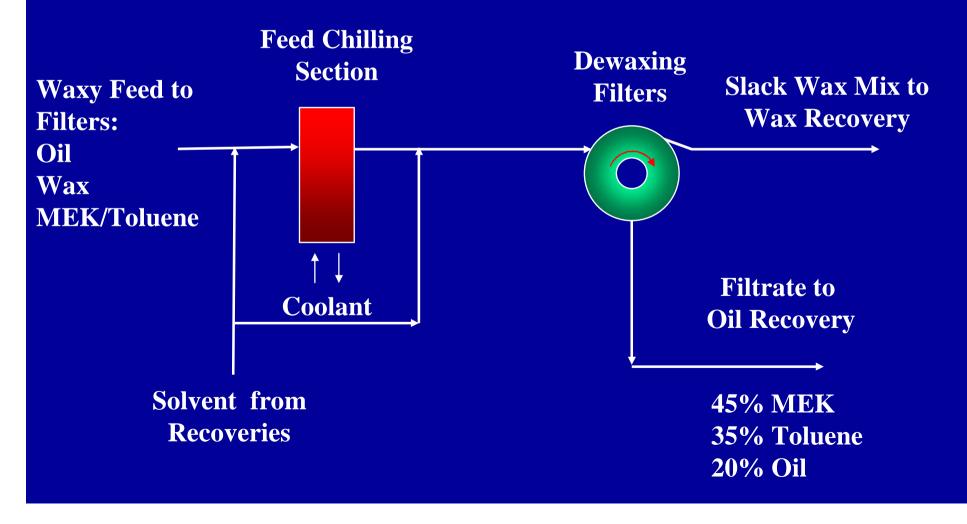
"Separation processes account for between 40-70% of both the capital and operating costs in industry"

Consider 1m3 of a dilute solution of solute in a solvent, which needs to be concentrated 10x.

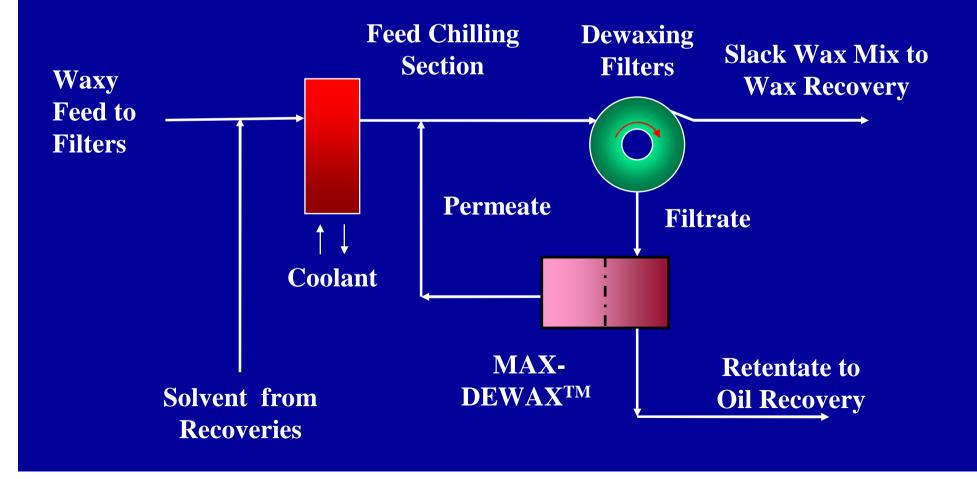
- Using distillation, $\Delta H_{fg} = 38 \text{ MJ kmol}^{-1}$, MW = 50 g mol}{-1} and $\rho = 800 \text{ kg m}^{-3}$
 - Evaporation requires 550 MJ heating
 - Condensation requires 550 MJ cooling
- Using OSN, applied pressure = 30 bar
 - Pump energy required = 3 MJ
- Given high energy prices here to stay, massive savings possible....

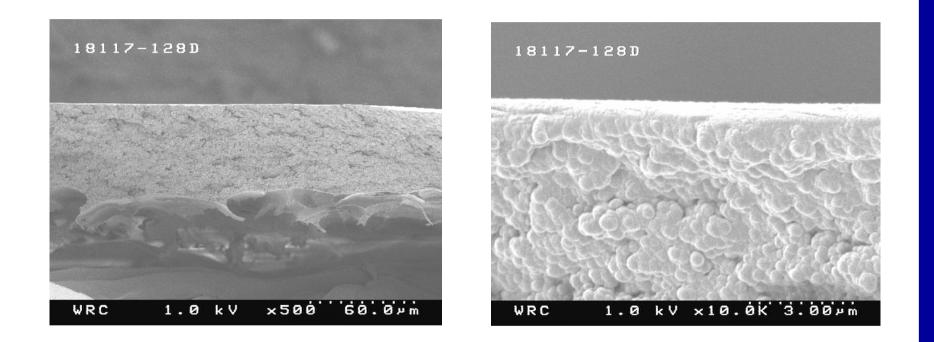
- Starting in 80's and 90's, oil majors (Exxon, Shell) and chemical companies (ICI, Union Carbide) began to file patents on the use of polymeric membranes to separate molecules present in organic solutions (lube oil recovery, aromatics enrichment, homogeneous catalyst recycle). They used existing commercial (aqueous) membranes, or made their own
- In the 90's, some major membrane producers (Grace Davison, Koch, Osmonics) began serious research programmes/made acquisitions and OSN products started to appear on the market
- These have prompted a rapid rise in the number of academic publications, and in process development projects in industry
- Largest success so far industrially has been WRGrace's Max-DewaxTM process

Conventional Solvent Dewaxing

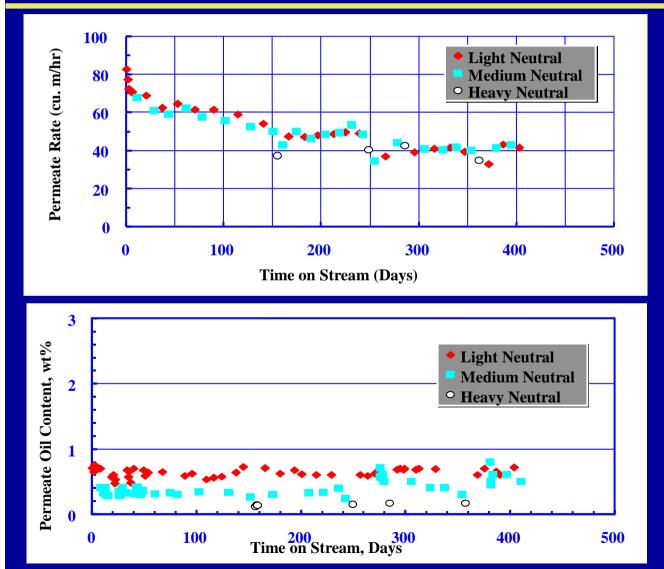


Solvent Dewaxing with Membranes – MaxDewaxTM





Grace Davison Membranes STARMEMTM polyimide membrane at 500x and 10,000x magnification of active separation layer.



Commercial Unit Permeate Production Typically 60 m³ h⁻¹

Commercial Unit Permeate Purity Feed filtrate typically 18-22wt% oil; Oil rejection 95-99%





10% expansion of lube and waxtrainProject cost \$6 million,Net benefit \$6 million per annum

MaxDeWaxTM Unit At ExxonMobil Beaumont Refinery Processes 11,000 m³ d⁻¹ solvent

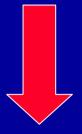


RESEARCH CHALLENGES IN OSN

- How can we characterise OSN membranes?
- How should we describe transport through OSN membranes?
- Can we find further applications where OSN can provide breakthroughs over current technology?
 - How do we improve stability of membranes to apply OSN to all solvents?
 Can we engineer the nanostructure so as to

engineer molecular weight cutoff/molecular discrimination?

Existing Membranes

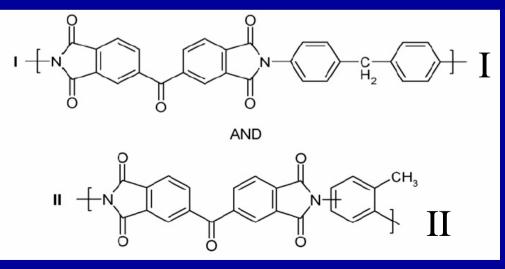


Next Generation Membranes

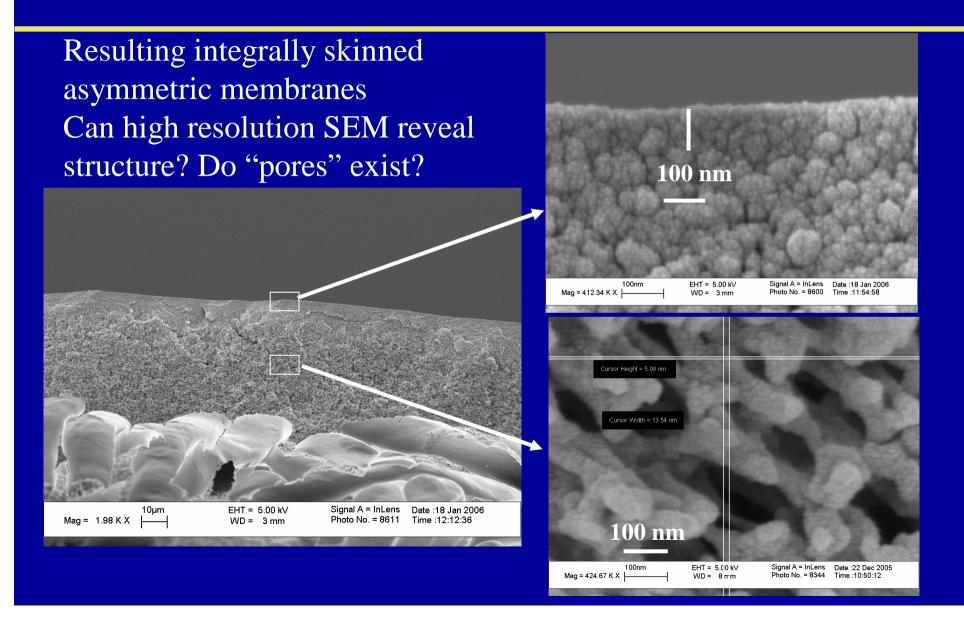
STRUCTURAL CHARACTERISATION

Can we relate any physically observable feature to performance ? STRATEGY

- Form membranes by phase inversion
- -Vary casting parameters to get functional performance changes
- -See if observed features correlate with performance change

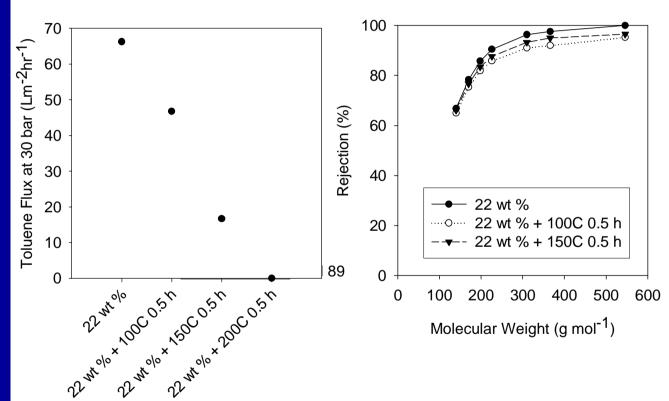


Lenzing P84 polyimide 20% I 80% II



Is the nodular structure viewed under SEM only an artefact of the SEM technique?

Effect of thermal annealing on flux.....



Flux and rejection of 22 wt % membranes at different thermal annealing temperatures.

Shows that nodular structure disappears with annealing.

So can see gross changes. Nodular structure exists....

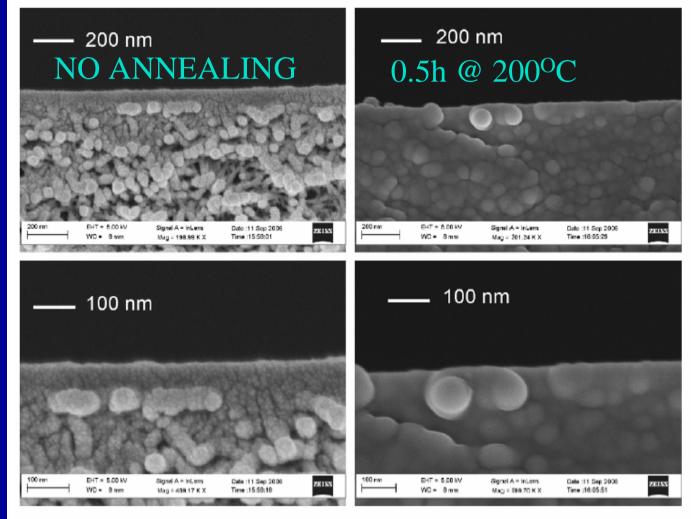
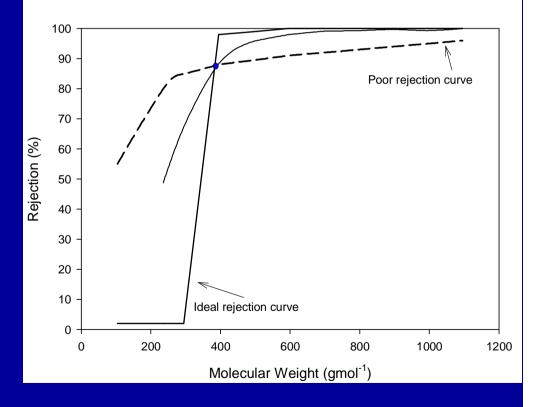


Fig. 12. Membrane morphology before (M2 left) and after annealing (M11) at 200 °C for 0.5 h.

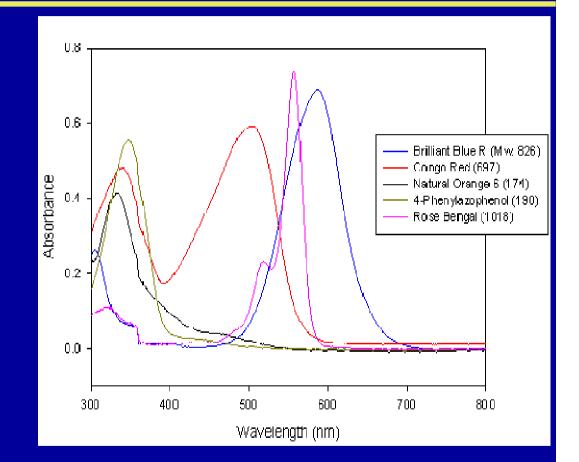
FUNCTIONAL CHARACTERISATION

- Many different solvent/solute combinations are used
- Most methods only provide a few or even just one point in the nanofiltration range 200 – 1000 gmol⁻¹
 - Alkanes, organic dyes, polymers, etc.



DYES

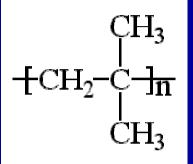
- Quick analysis using UV spectrophotometer
- Changes in concentration clearly visible
- Many dyes are charged or acidic
- Various non-uniform structures
- Spectrum overlap



UV spectrum for dyes with various MW

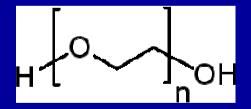
 Homologous polymers with steadily increasing MW

 eg: polyisobutylene, polyethylene glycol, sugars etc.



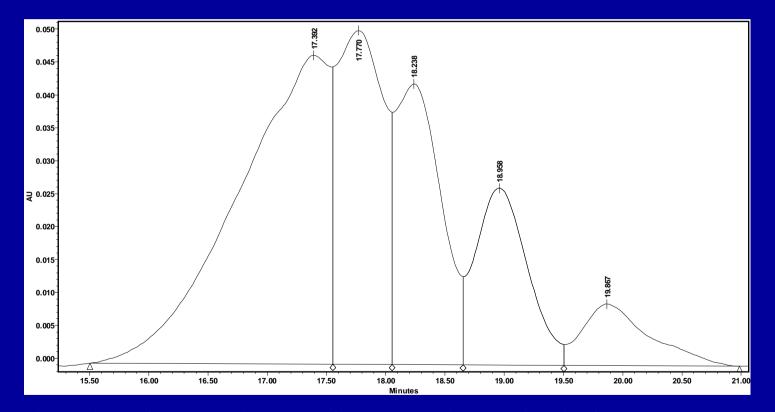
Polyisobutylene

 Analysis with size exclusion chromatography requires de-convolution of overlapping peaks



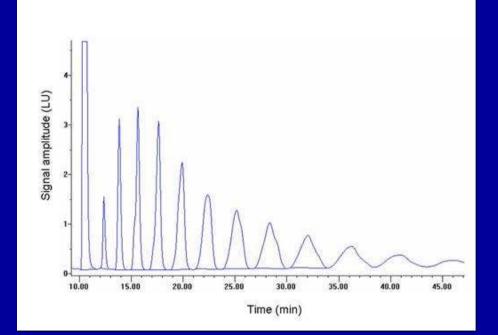
Polyethylene glycol

• Typical size exclusion chromatography trace of polystyrene



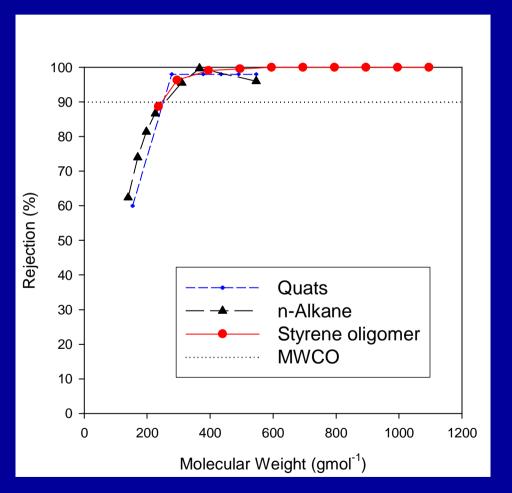
 Overlapping peaks require complex calculations to separate each species

- We have developed a simple and reliable method using styrene oligomers obtained from Polymer Labs, UK
 Styrene oligomers easily detected using UV-vis at a wavelength of 264 nm
- Separation of test species achieved using liquid chromatography employing a conventional reverse phase C18 column
- Mobile phase H₂O to tetrahydrofuran 35:65 by volume



 $-CHCH_2$

- Validation of oligostyrene test comparing to other established methods and results
- Filtrations performed in toluene @ 30 bar pressure
- STARMEMTM122 has been characterised across the entire nanofiltration range



Molecular weight cutoff curve for ST 122

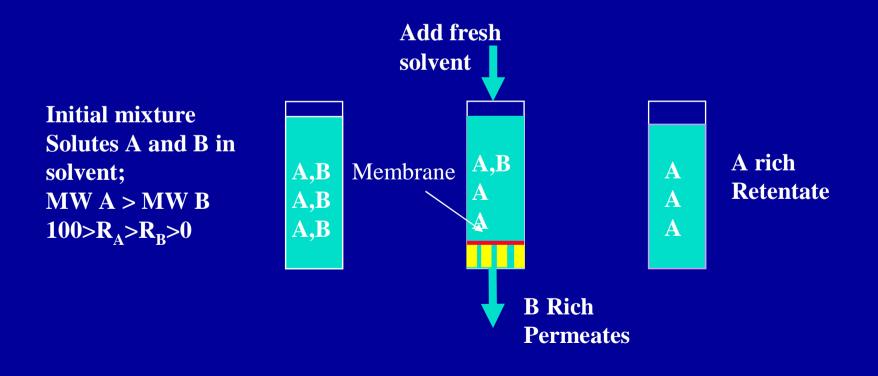
Organic Solvent Nanofiltration OSN Applications

"The best way to have a good idea is to have a lot of ideas" – Linus Pauling Potential Applications of OSN

- Concentration of Solutes in Solvents
- Solvent Exchanges (high-boiling solvent to a low boiling solvent)
- Purifications separation of high and medium MW species in solvent
- Catalyst Recycle and Re-Use
 - Phase transfer catalysts (re–use catalysts, separate catalysts from products)
 - Organometallic catalysts recovery and reuse (re-use ligands, avoid metal contamination of product)
 - Ionic Liquid Mediated Catalytic Reactions
- Dynamic Kinetic Resolution (separated catalyst systems)
- Chiral separations (host-guest interactions)
- Biotransformations
- Natural Oils Processing

Organic Solvent Nanofiltration in Chemical Processes OSN Applications

Constant Volume Membrane Purification Solute (API) is added as a batch at start of process Solvent is added continuously to make up for solvent permeating across the membrane – therefore volume in system stays constant



Organic Solvent Nanofiltration OSN Applications

Constant Volume Diafiltration to separate model active pharmaceutical ingredient (API -Yellow) from model large impurity ie dimer/trimer (Blue). Solvent is Methanol



FEED – mixture of blue and yellow dyes



Organic Solvent Nanofiltration OSN Applications

 Example – Separation of coloured impurity from API at Astra Zeneca by OSN (The Chemical Engineer, August 2006)

- 3(a) Starting material containing high MW colour compound
- 3 (b) Downstream issues caused by impurities
- Nanofilter solution so that API passes through membrane with solvent, impurity is retained
- 3 (c) Product after OSN purification – nice white powder!



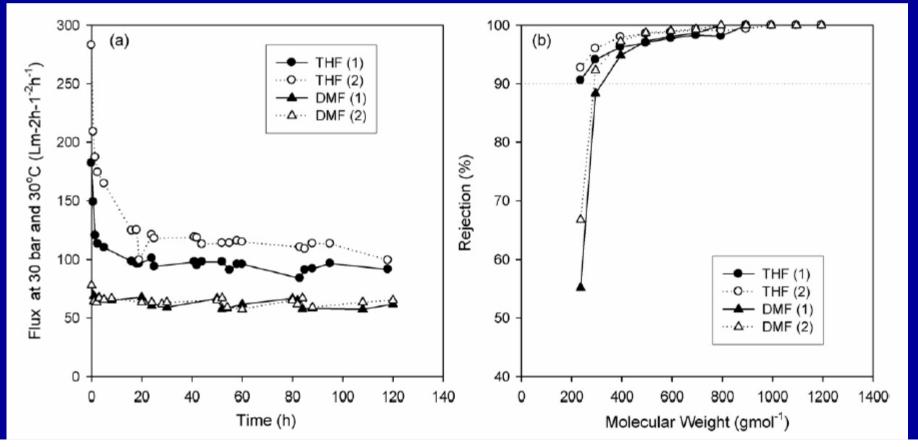
Organic Solvent Nanofiltration Next Generation Membranes

Challenges for new membranes

- Membranes Stable in "tough" solvents eg acetone, DCM, DMF, THF, NMP
- Tunable molecular weight cutoff profiles

Organic Solvent Nanofiltration Next Generation Membranes

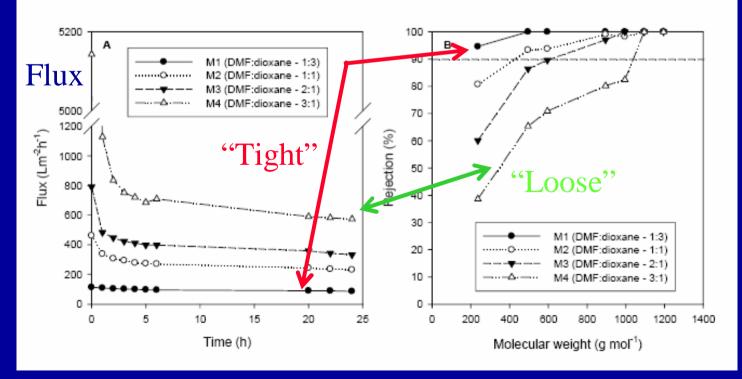
Post-formation cross-linking of polyimide membranes Resulting membranes have excellent stability and flux in "tough" solvents such as DMF! (data below collected at 30 bar, 30°C)



Organic Solvent Nanofiltration Next Generation Membranes

Tunable Molecular Weight Cutoff Profile

- Found that the main variable which could provide significant changes in the profile was the solvent/volatile co-solvent ratio
- Using P84 and DMF (solvent) Dioxane (co-solvent)



Organic Solvent Nanofiltration Technology Transfer

SO WHAT?

United States Patent [19] Livingston

Economist.com

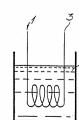
May 24th-30th 1997 Economics Focus Playing godmother to invention "Many countries spend heavily to foster research and development. But inventing new technology is less important than using it effectively."

USE IT – OR LOSE IT!

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[73] Assignee: Imperial College of Science Technology & Medicine, London, Great Britain		
[21]	Appl. No.:	211,159
[22]	PCT Filed:	Sep. 18, 1992
[86]	PCT No.:	PCT/GB92/01719
	§ 371 Date:	Jun. 10, 1994
	§ 102(e) Date:	Jun. 10, 1994
[87]	PCT Pub. No.:	WO93/06045
PCT Pub. Date: Apr. 1, 1993		
[30]	Foreign A	pplication Priority Data
Sep. 18, 1991 [GB] United Kingdom		
 [51] Int. Cl.⁶		
[58]	Field of Searc	210/500.23; 210/909 h 210/321.87, 500.21,
210/615, 651, 909, 500.23		
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Primary Examiner—Robert A. Dawson Assistant Examiner—Kenneth M. Jones Attorney, Agent, or Firm—Fay, Sharpe, Beall, Fagan, Minnich & McKee

ABSTRACT

A method of reducing the concentration of at lesst one organic compound present in an aqueous feeddock, wherein said feedstock is supplied to one side of a substantially water-insoluble selectively permeable polymetic sheet or tubular membrane whose permeability to the or each said organic compound exceeds its permeability to tohoride ion whilst simultaneously maintaining in contact with the other side of said membrane an aqueous reaction medium containing biologically active reaction means capable of reaching with said at lesst one compound after it permeates through the wall of the tubular membrane. Apparetus, prefearbly enclosed, for carrying into effect the method is also disclosed and permits treatment of waste waters containing volatile organic compounds. Modular biomester organeratus in the form of a cartridge containing a bundle of polymeric membrane tubes is also disclosed.

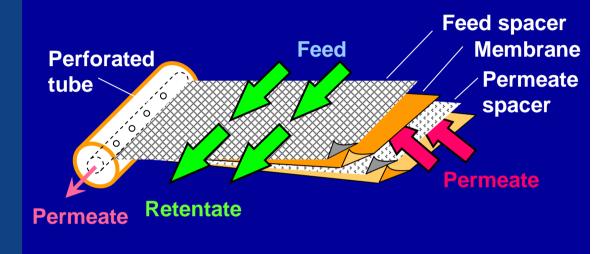
36 Claims, 6 Drawing Sheets

Organic Solvent Nanofiltration OSN Commercial



- Membrane Extraction Technology started as Spin Out Company from Imperial College in 1996, now based in West London
- MET delivers "innovation to operation" on new separation technologies (equipment, process development, membranes)
- Technology Platforms
 - Selective extraction of organics from aqueous streams
 - Molecular separation in organic solvents (Organic Solvent Nanofiltration, OSN)
- MET provide WR Grace STARMEMTM series of polyimide OSN membranes to chemical and pharmaceutical industry
 - Crosslinked membranes licensed to MET for commercialisation

Organic Solvent Nanofiltration OSN Commercial



Scale up membrane formation and develop appropriate spiral module fabrication
 DuraMemTM range of highly stable OSN membranes launched by MET in 2008
 First installation made at process scale in "large pharma" plant April 2008



Organic Solvent Nanofiltration SUMMARY

- Organic solvent nanofiltration (OSN) has already reached large scale in refining operations
- Major challenges remain for technology to make paradigm shift
- We are still seeking ways to observe the detailed physical nanoscale structure of separating layer
- Transport mechanisms still under investigation
- A new generation of highly stable membranes with tuneable molecular weight cutoff curves – DuraMemTM - has been created

Organic Solvent Nanofiltration Acknowledgements

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- Lloyd S. White W.R.Grace and Co, MD, USA; Craig Wildemuth Grace Davison Membranes, CO, USA
- UK Engineering and Physical Sciences Research Council, European Commission

